

Supporting Information

for

Facile synthesis of Fe-based metal–organic frameworks from Fe_2O_3 nanoparticles and their application for CO_2/N_2 separation

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Additional experimental data

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Preparation of the reference MIL-100(Fe) sample

The reaction mixture was prepared with a molar composition of 1.0 Fe: 0.67 H₃BTC: 1.2 HNO₃: 2.0 HF: 280 H₂O in a 100 mL Teflon-lined autoclave. It was stirred for 20 min at ambient temperature. Subsequently, the mixture was tightly sealed and incubated at 160 °C for 24 h in an electric oven. Afterward, it was cooled down to room temperature. The MIL-100(Fe) was then retrieved from the orange slurry after centrifugation and subjected to multiple washes with dimethylformamide and ethanol to eliminate any residual reactants from the product mixture. Finally, the MIL-100(Fe) was left to dry overnight at 70 °C.

Samples	The obtained parameters from fitting CO ₂			
	$q_{\rm sat}({\rm mmol}\cdot{\rm g}^{-1})$	a (kPa ⁻¹)	п	R^2
M-100Fe@Fe ₂ O ₃ #0.90	3.59748	0.00225	0.96613	0.9999
M-100Fe@Fe ₂ O ₃ #1.35	4.47178	0.0035	0.91115	0.9999
M-100Fe@Fe ₂ O ₃ #1.80	5.75658	0.00417	0.87543	0.9998
M-100Fe@Fe ₂ O ₃ #2.25	6.31350	0.00446	0.8521	0.9998
MIL-100(Fe)	5.29325	0.00873	0.86948	0.9998

Table S1: The characteristic parameters alongside correlation coefficients from fitting the

 Langmuir–Freundlich (L–F) model.

Samples	The obtained parameters from fitting N ₂				
	$q_{\rm sat}({\rm mmol}\cdot{\rm g}^{-1})$	a (kPa ⁻¹)	п	R^2	
M-100Fe@Fe ₂ O ₃ #0.90	0.48828	0.00143	1.02837	0.9998	
M-100Fe@Fe ₂ O ₃ #1.35	0.97068	0.00123	0.94648	0.9999	
M-100Fe@Fe ₂ O ₃ #1.80	1.28516	0.00119	0.94557	0.9999	
M-100Fe@Fe ₂ O ₃ #2.25	1.60773	0.00111	0.91890	0.9999	
MIL-100(Fe)	0.65055	0.00372	0.97849	0.9998	

The Langmuir–Freundlich (L–F) model is described as the following equation [1,2]:

$$q = q_{\text{sat}} \frac{ap^n}{1+ap^n} \tag{1}$$

Where $q \pmod{g^{-1}}$ stands for the uptake amount; $q_{sat} \pmod{g^{-1}}$ stands for the saturation uptake capacity on the adsorptive sites; $p \pmod{p}$ is the pressure of bulk gas at equilibrium with the adsorbed phase; $a \pmod{p^{-1}}$ is the affinity coefficient of the sites; n is the coefficient of the L–F model. The CO₂/N₂ selectivity was calculated using the formula as below [3]:

$$S_{\rm CO_2/N_2} = \frac{q_{\rm CO_2}/p_{\rm CO_2}}{q_{\rm N_2}/p_{\rm N_2}}$$
(2)

Where q_{CO2} and q_{N2} are loading amounts of CO₂ and N₂ in mmol g⁻¹ estimated by IAST,

respectively. p_{CO2} and P_{N2} are the partial pressure of CO₂ and N₂ in kPa, respectively.

The Clausius–Clayperon equation is described as the following equation [1,4]:

$$lnP = -\frac{Q_{st}}{RT} + C \tag{3}$$

Herein, P is the pressure in kPa, R is the ideal gas constant in $J \mod^{-1} K^{-1}$, T is the absolute

temperature in K, and C is the constant in the dimensionless unit.

Adsorbents	Adsorption capacity $(mmol \cdot g^{-1})$	Temperature (K)	References
ZSM-5	1.50	303	[5]
MCM-41	0.79	298	[6]
Mesoporous alumina	1.18		
SBA-15	0.47	298	[7]
γ-Alumina	0.68		
Zeolite-13X	1.70	208	[8]
ZIF-8	0.83	290	
ZIF-70	1.43	298	[9]
UIO-66	1.79	298	[10]
d-UiO-6-2.0HCl	1.42	298	[11]
UiO-66_FA_mod	1.44	298	[12]
MF-MOF-801	1.37	200	[12]
MF-MOF-804	1.00	298	[15]
MW-MIL-100(Fe)	$1.50 (1981 \text{ m}^2 \cdot \text{g}^{-1\#}; 250 \text{ °C}^{\bullet})$	298	[14]
MIL-100(Fe)	$1.29 (1107 \text{ m}^2 \cdot \text{g}^{-1\#}; 120 ^\circ\text{C})$	298	[15]
MIL-100(Fe)	$0.92 (1083 \text{ m}^2 \cdot \text{g}^{-1\#}; 150 ^\circ\text{C})$	298	[16]
MIL-100(Fe) M-100Fe@Fe2O2 $\#1.80$	1.77 ($1825.4 \text{ m}^2 \cdot \text{g}^{-1\#}$; 150 °C*)	298	This work
$10110010010203\pi1.00$	1.11 (1505.4 m·g *, 150 °C)		

Table S2: Compared CO₂ uptake capacity on various adsorbents at 1 bar.

[#]BET surface area; *Activation temperature before measuring CO₂ adsorption capacity over the

absorbents



Figure S1: CO₂ isotherms at several different temperatures on M-100(Fe)@Fe₂O₃#1.80 sample.



Figure S2: EDX mapping of elemental Fe and C on the M-100Fe@Fe2O3#1.80 sample

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